

Low-Pressure Membrane Contactors for Carbon Dioxide Capture DE-FE0007553

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NETL CO₂ Capture Technology Meeting
Wednesday, July 10, 2013

Membrane Technology and Research

MTR designs, manufactures, and sells membrane systems for industrial gas separations



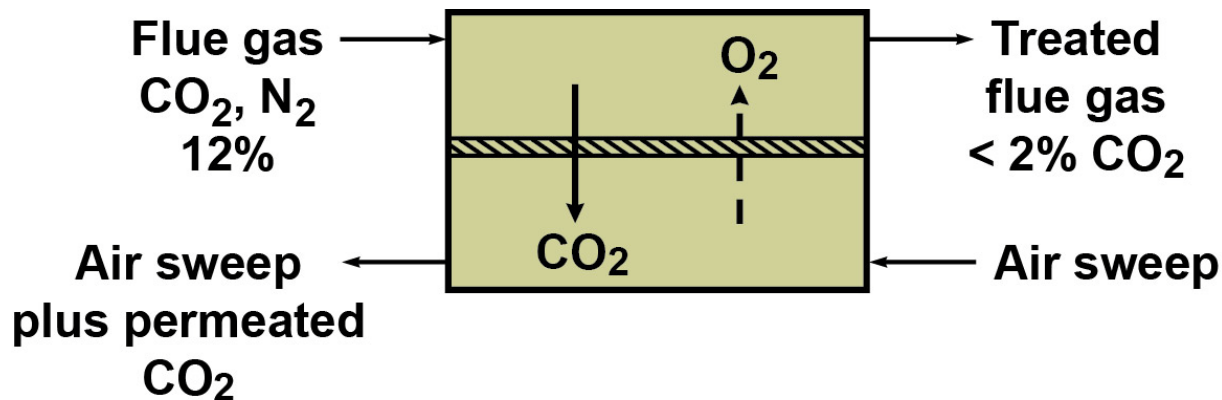
-70 Employees
-2012 Sales: \$25 million

Project Overview

- **Award name:** Low-pressure Membrane Contactors for CO₂ Capture
- **Project period:** 10/1/11 to 9/30/14
- **Funding:** \$ 3.0 million DOE; \$1.0 million MTR
- **DOE program manager:** Mike Mosser
- **Participants:** MTR, University of Toledo
- **Project scope:** Develop compact large membrane area (> 500 m²), low pressure drop plate-frame sweep module for CO₂ capture application
- **Project plan:** The key project work organized by budget period is as follows:
 - BP1 : Construct prototype laboratory modules (20m²), select components, develop fabrication technology.
 - BP2: Scale up production to 1m x 1m pilot scale modules (100m²), demonstrate with lab test system that modules meet CO₂ separation performance and pressure drop targets.
 - BP3: Scale up to full scale module (> 500 m²), show modules meet all performance targets. Be ready to test at NCCC.

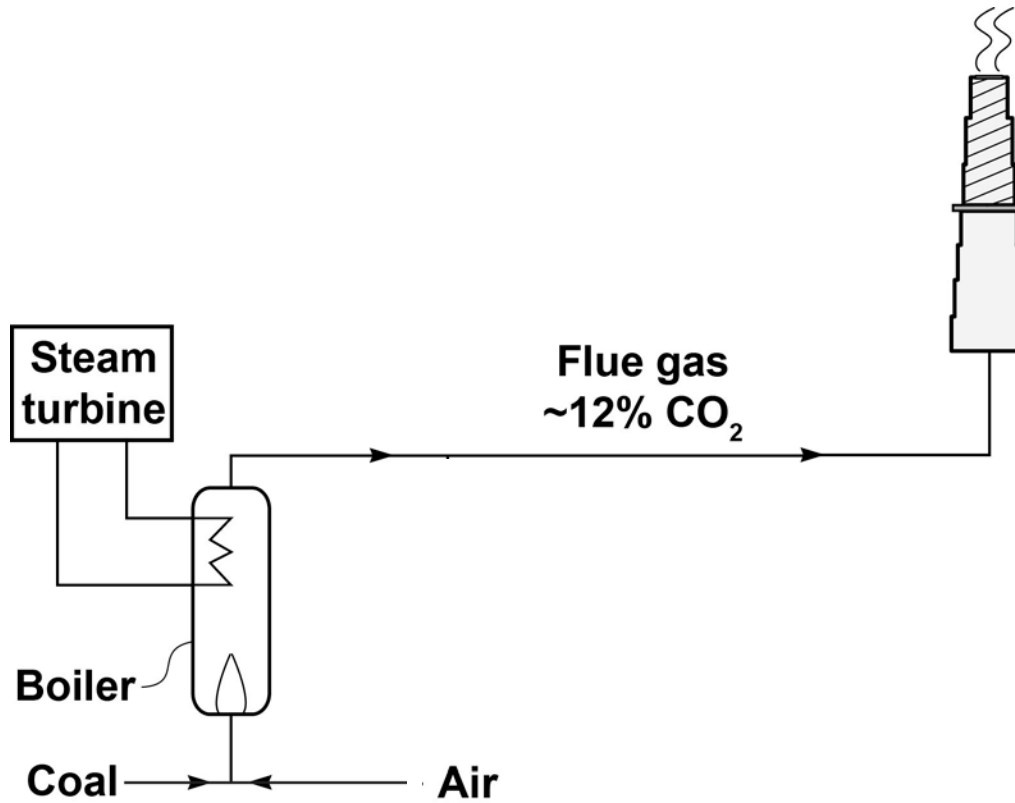
The MTR Membrane Contactor

A Way of Generating an Affordable (Partial) Pressure Difference

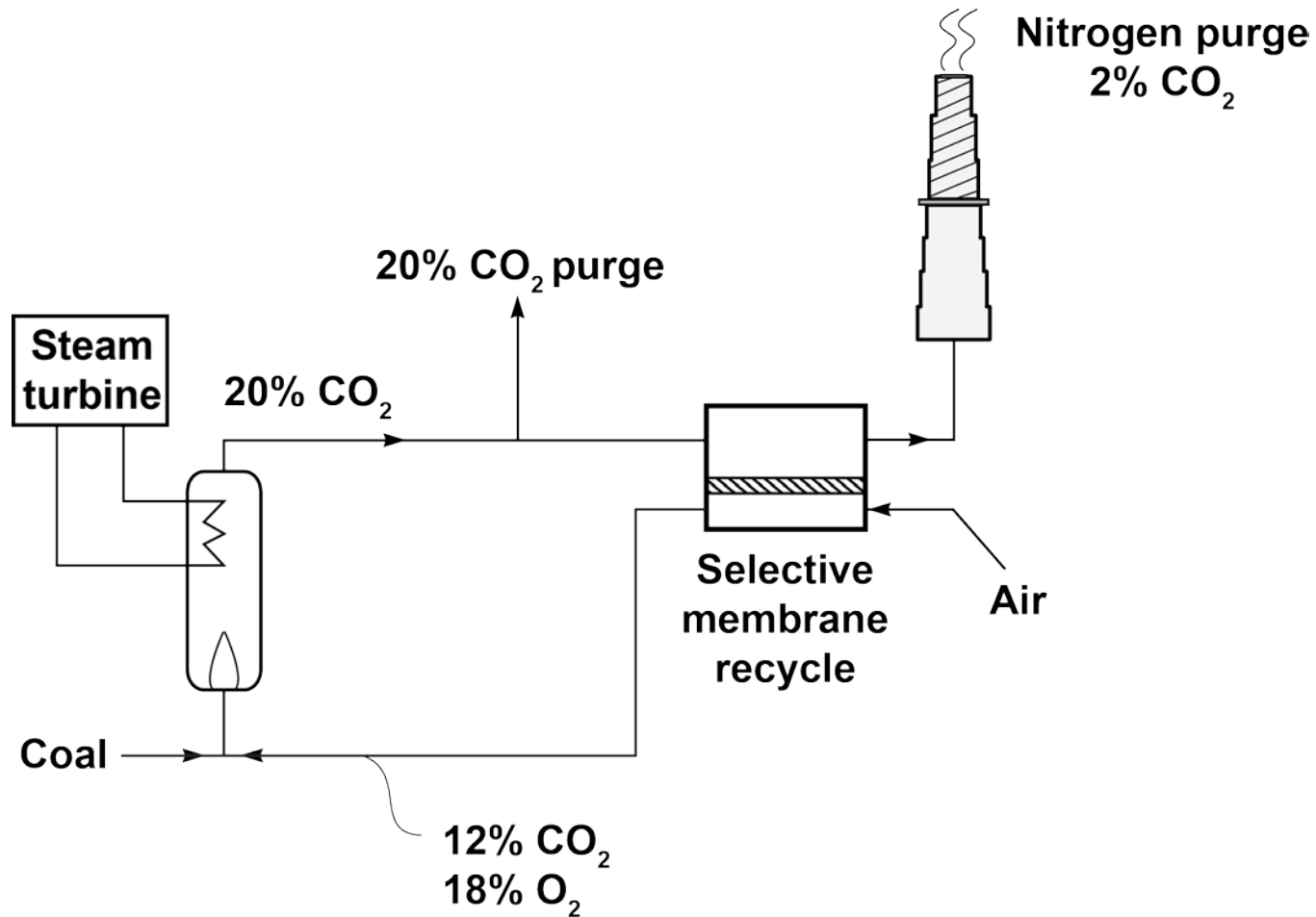


A separation is performed at a minimal energy cost

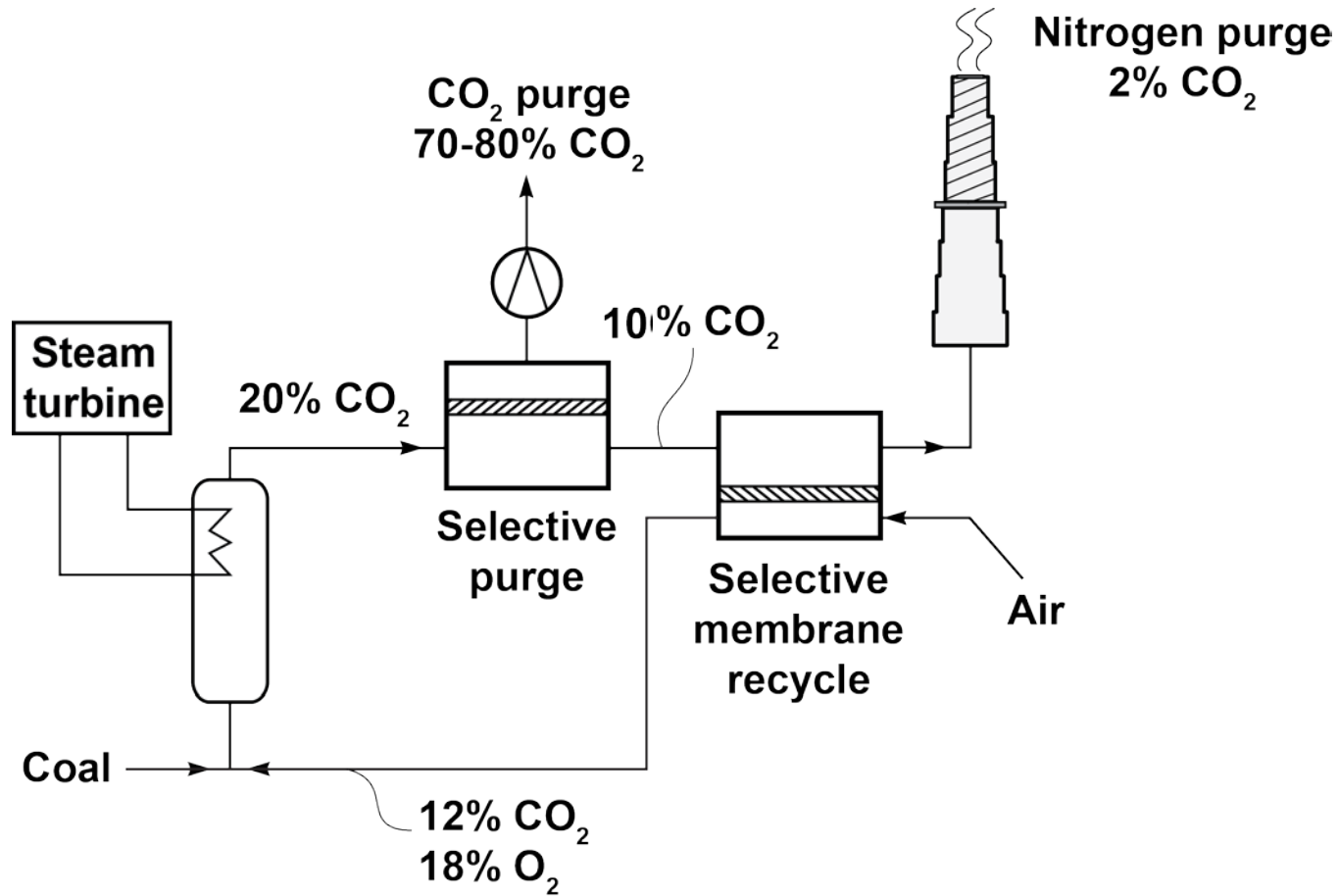
A Coal Power Plant



A Membrane CO₂ Pre-Concentrator



MTR's Membrane Solution



500 MW_e plant requires one million m² of membrane

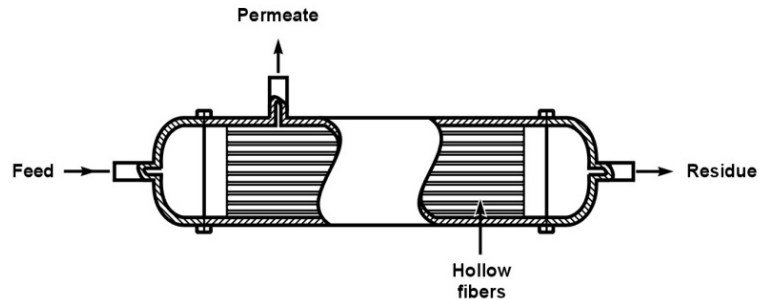
The Issues and Solutions

Membrane module area and cost are not an issue

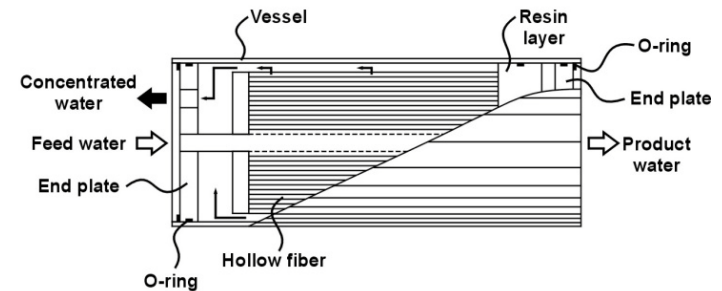
- Skid packing density
 - Manifolding
 - Footprint
 - A sweep process
 - Needs low pressure drop
- Large area modules,
compact skids
- Needs wide, straight
channels on both sides
of the membrane

Membrane Module Designs in Current Use

Capillary Fibers



Hollow Fine Fibers



Spiral-Wound Modules

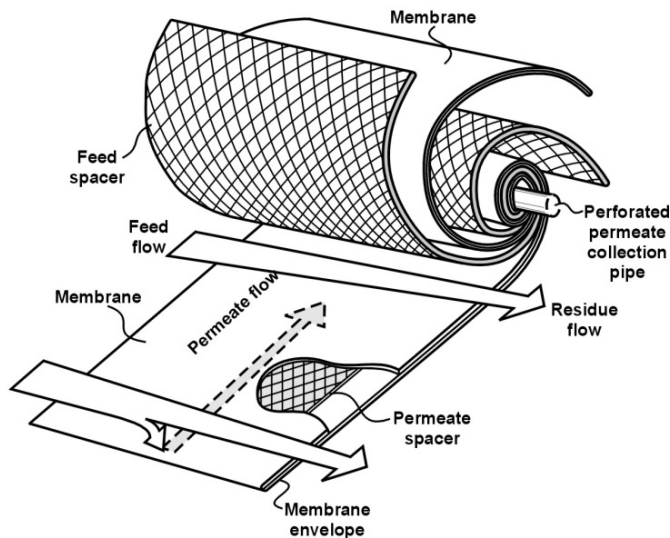
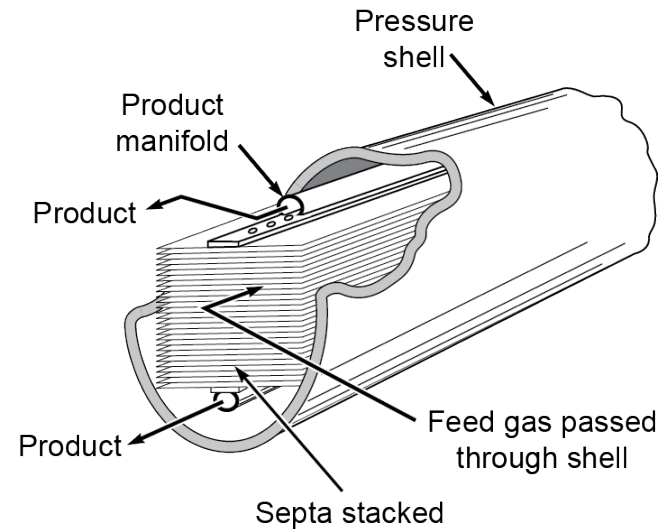
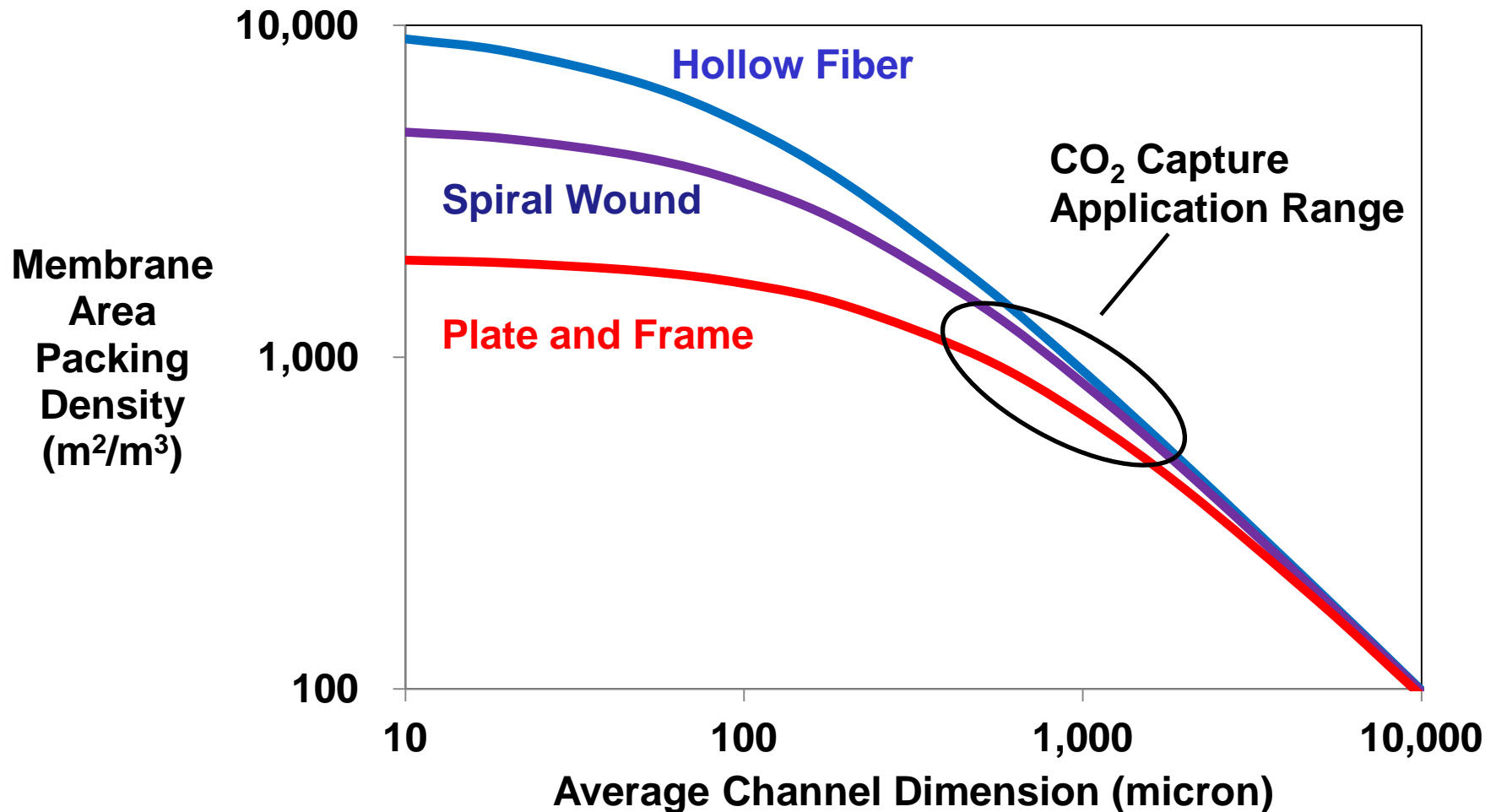


Plate-and-Frame Modules



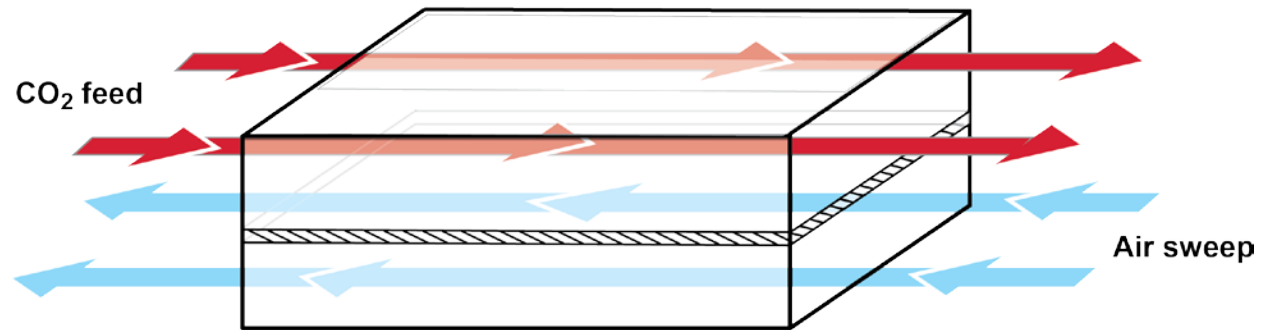
Packing Density for Different Membrane Module Configurations



Two Membrane Contactor Designs

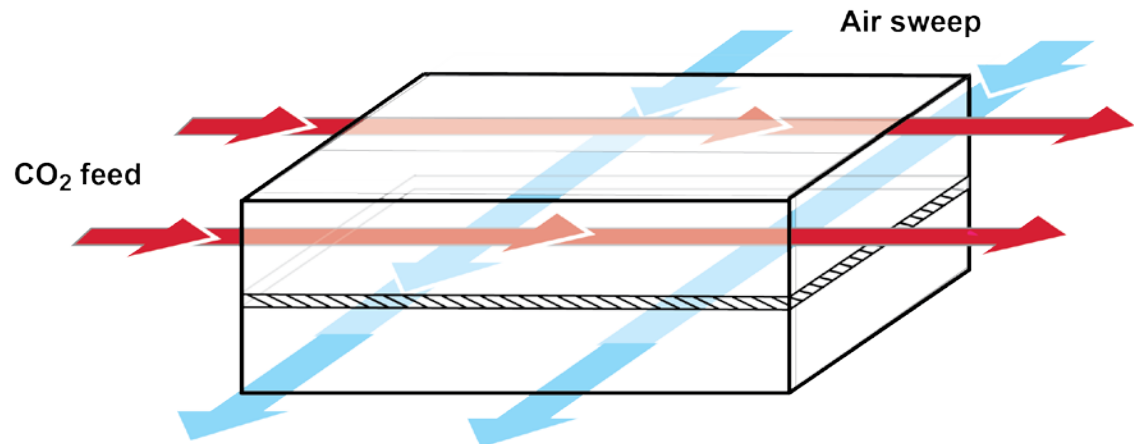
Countercurrent

- Most efficient
- Difficult to make



Cross-flow

- Uses 40% more membrane area
- Easier to make



Progress to Date

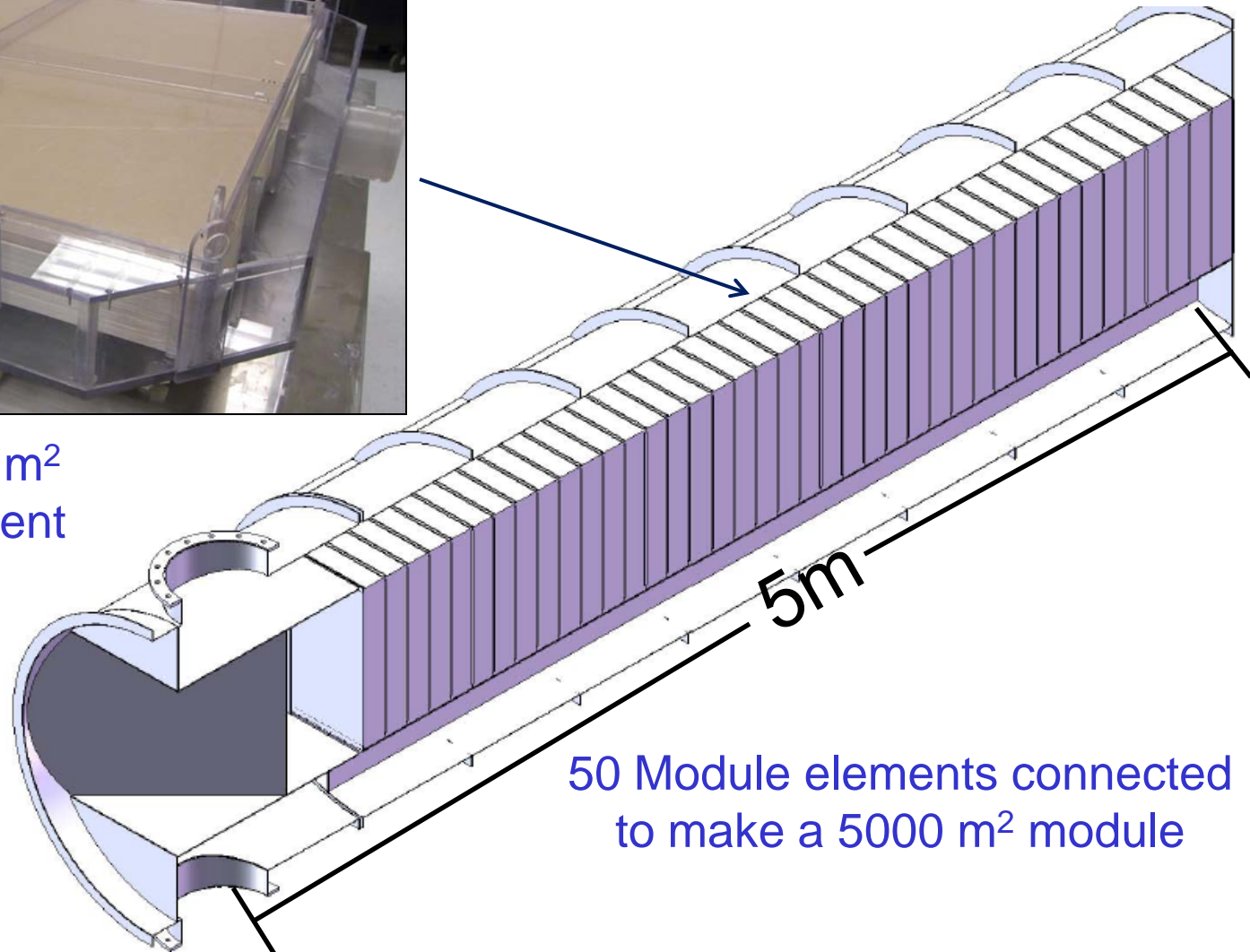
- **Year 1**
 - Footprint:
1ft x 2 ft
 - Modules:
20 m²
- **Year 2**
 - Footprint:
1m x 1m
 - Modules:
100 m²



Our Concept

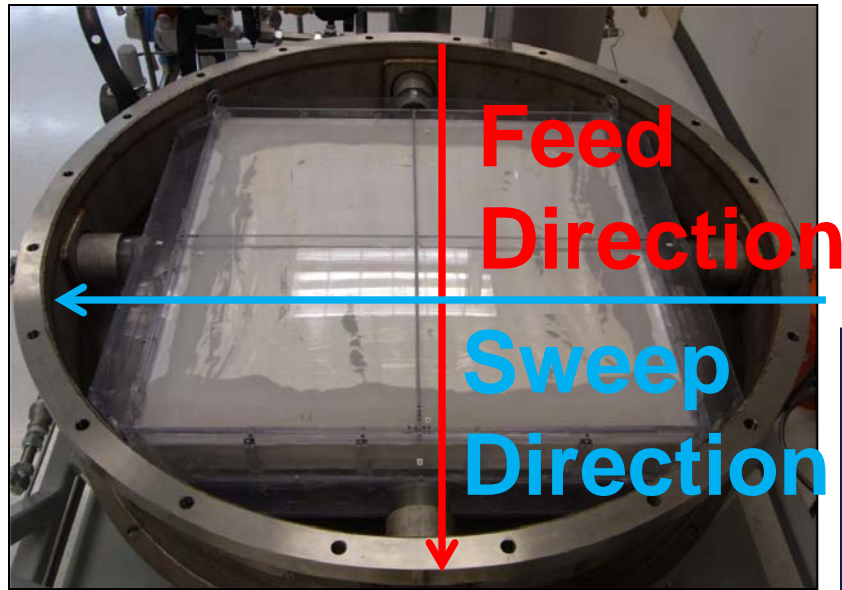


A single 100 m²
module element



50 Module elements connected
to make a 5000 m² module

Membrane Module and Test System

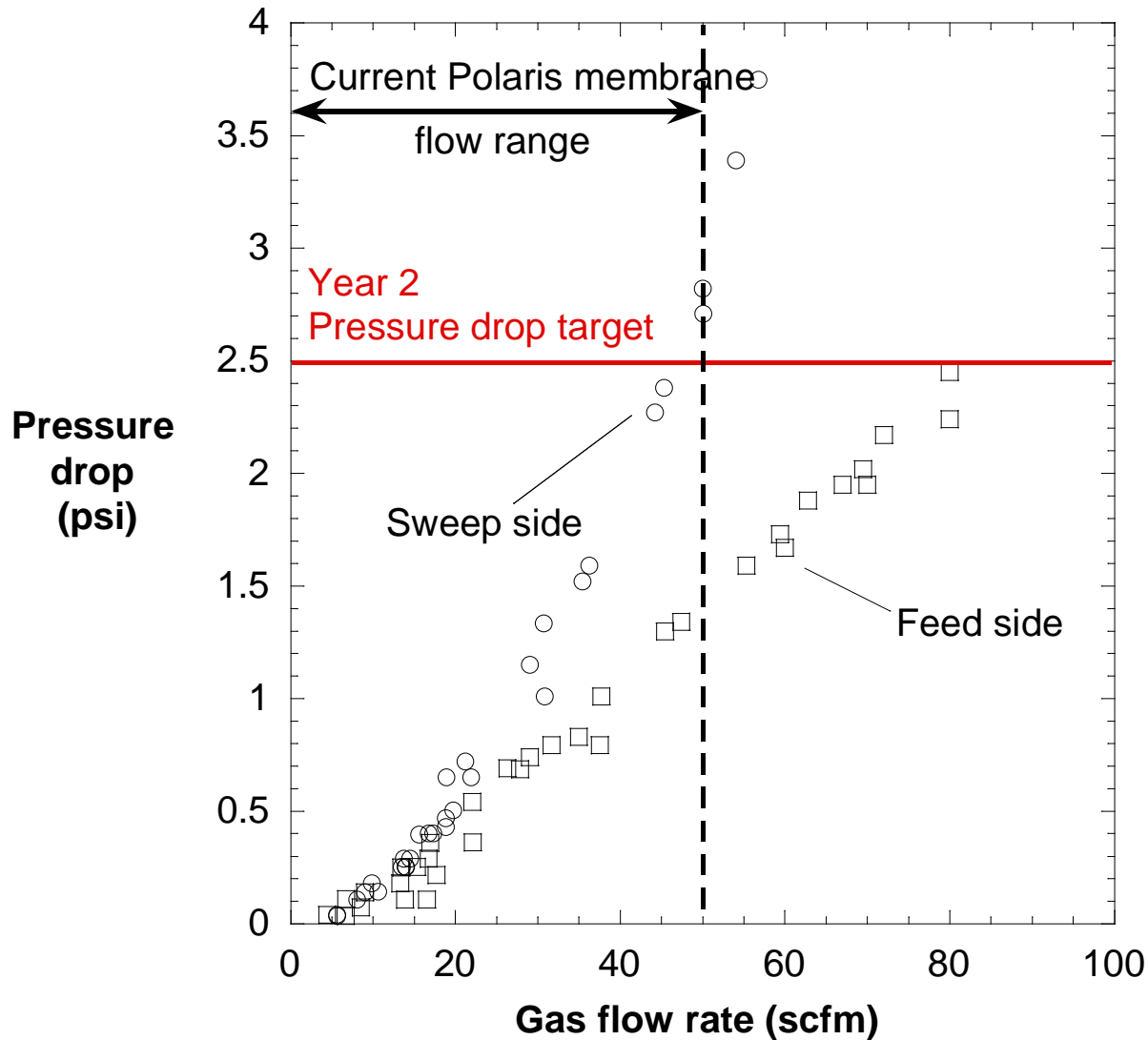


Membrane Contactor
with Vessel

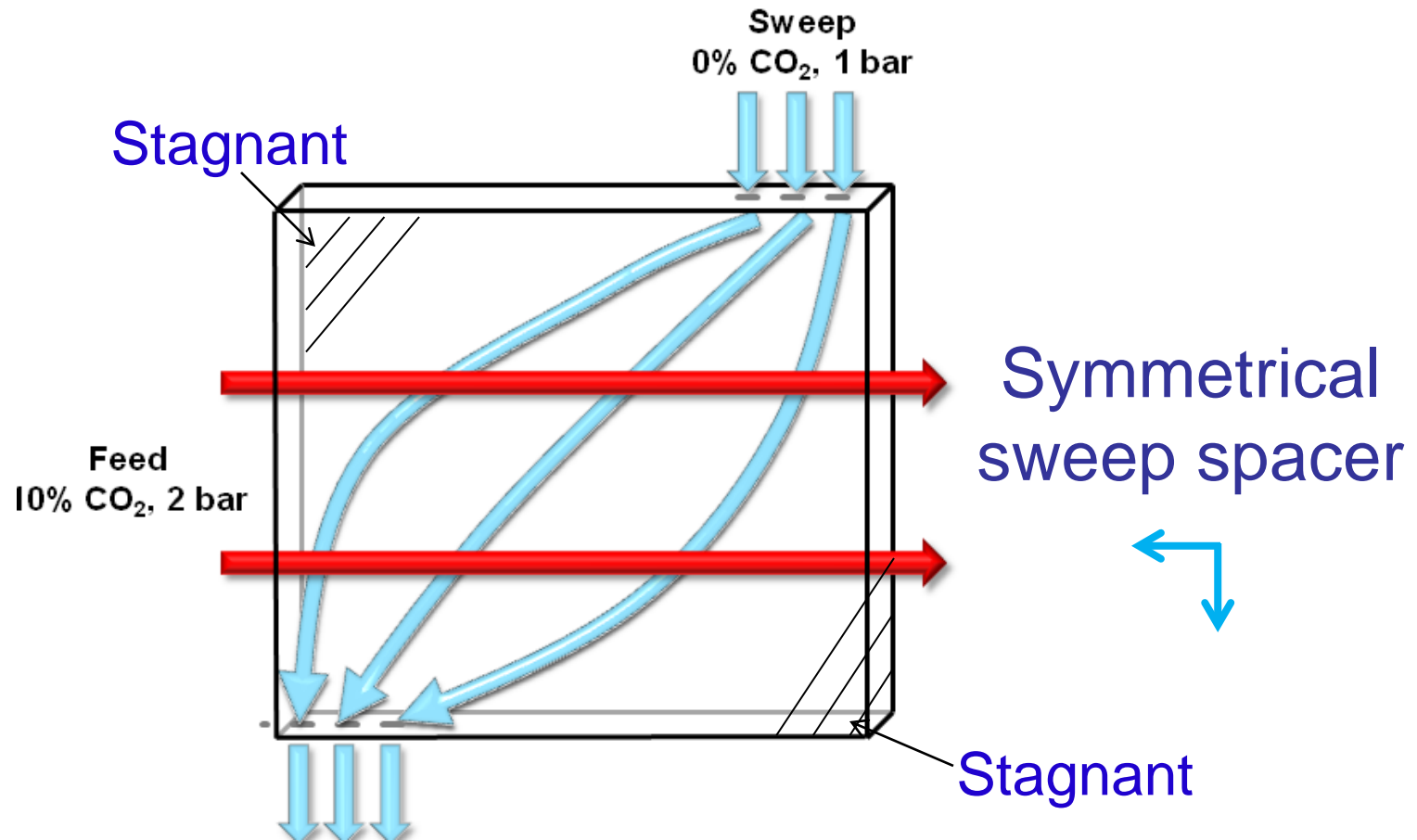
Test System



Module Pressure Drop within Target Range

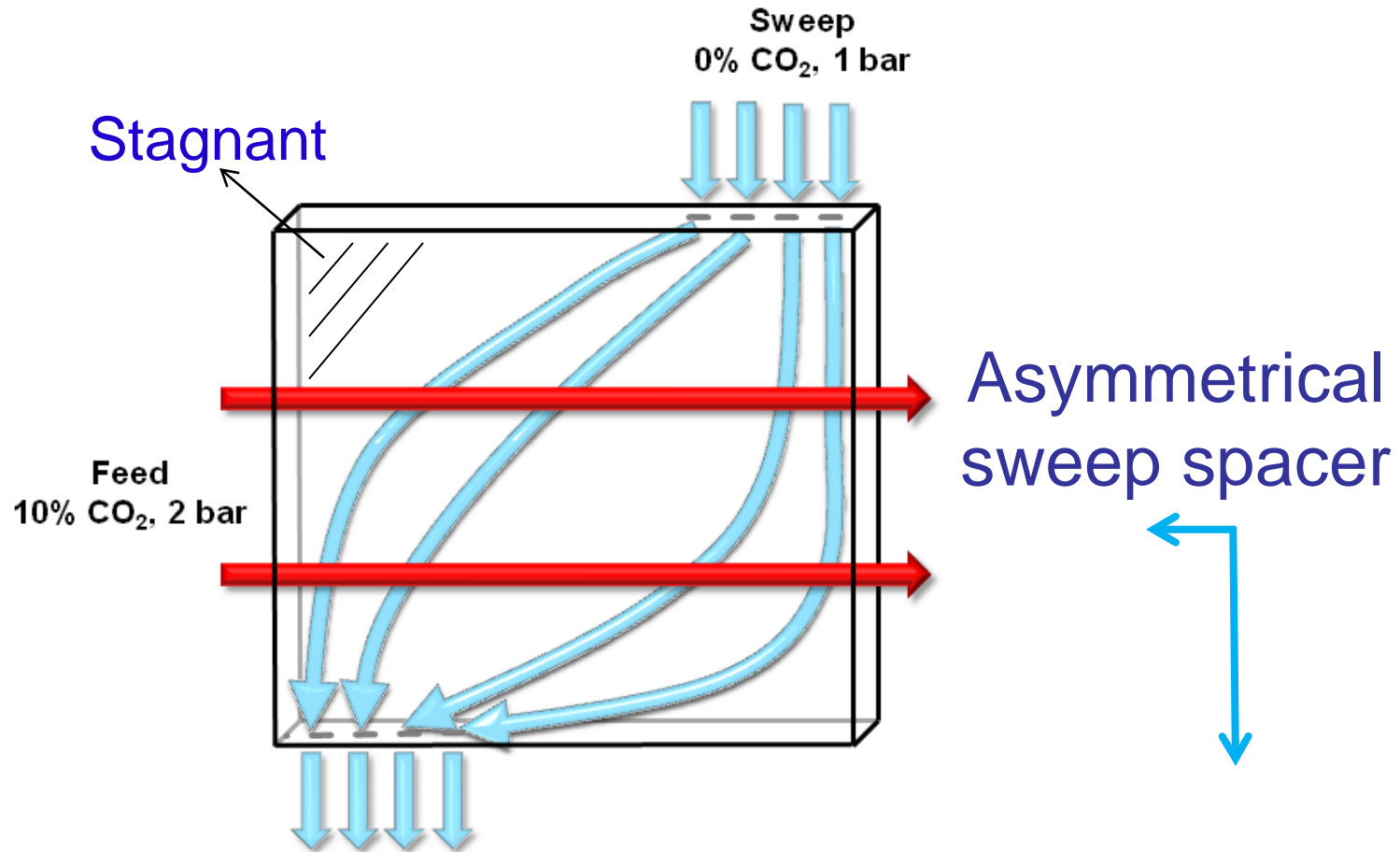


Partial Countercurrent Design



Needs **30%** more membrane compared to countercurrent

Partial Countercurrent Design



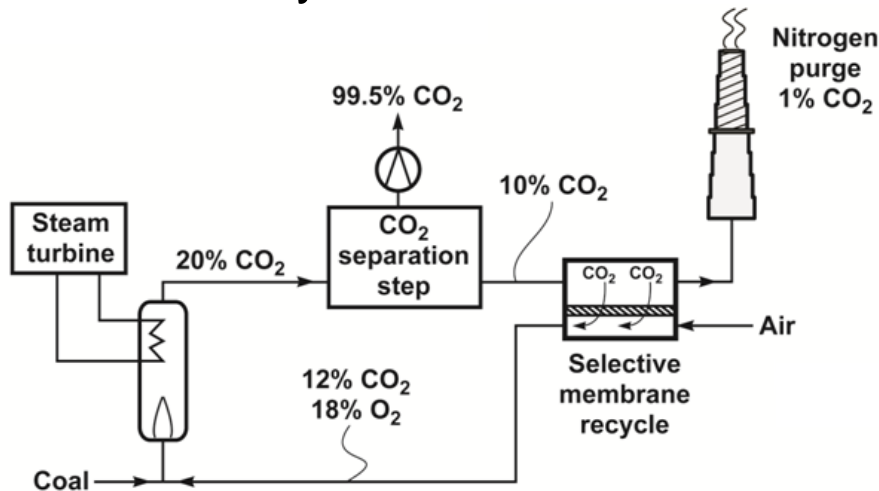
Needs **18%** more membrane compared to countercurrent

Our Plans

- Refine module fabrication techniques
- Improve module flow design
- Develop multi-element modules (3~5 elements)
- Test modules at NCCC (2014)

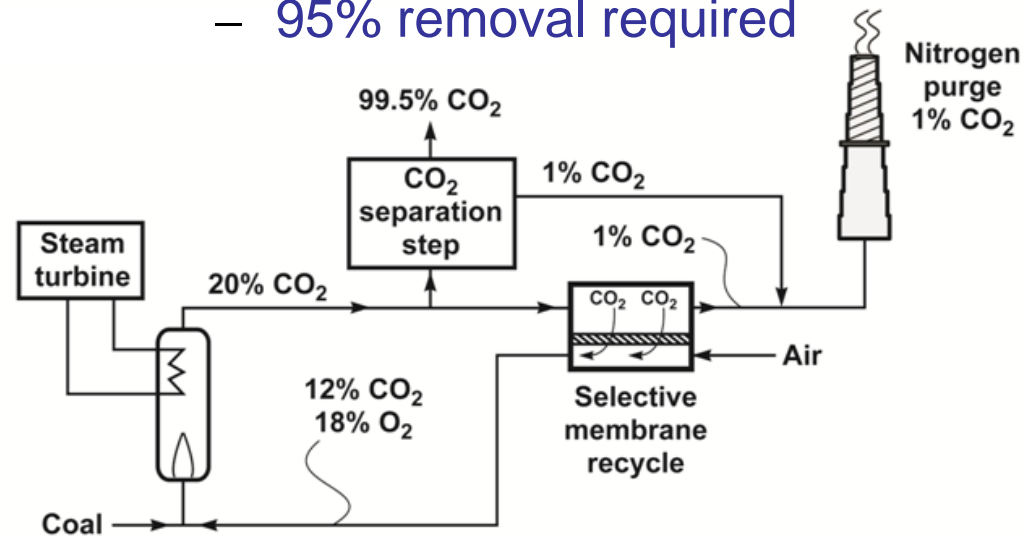
Combination Process May Be the Way to Go

Series Hybrid Case



- Double the CO₂ concentration
- 50% removal required

- Double the CO₂ concentration
- Half the flow
- 95% removal required



Parallel Hybrid Case